

# Impact of Surface and Physical Property on Rayleigh Taylor Instability in Sealed Vessel

Mehedi Tusar

Advisor: Dr. Shoaib Usman, Co-Supervisor: Dr. Syed Alam

Nuclear Engineering

# Background

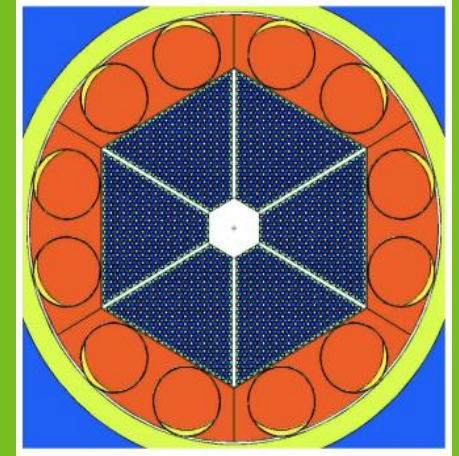
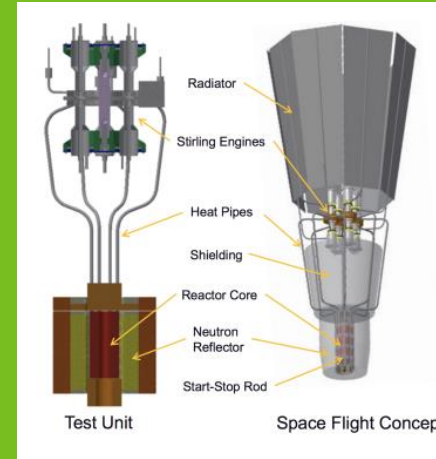
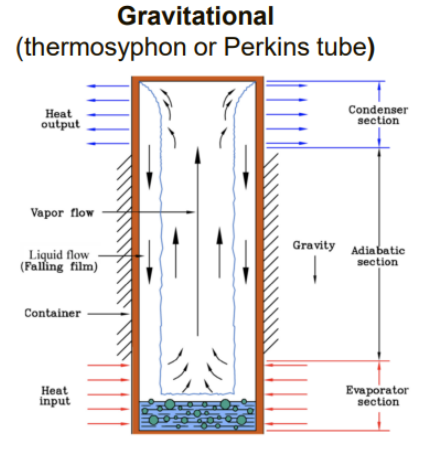
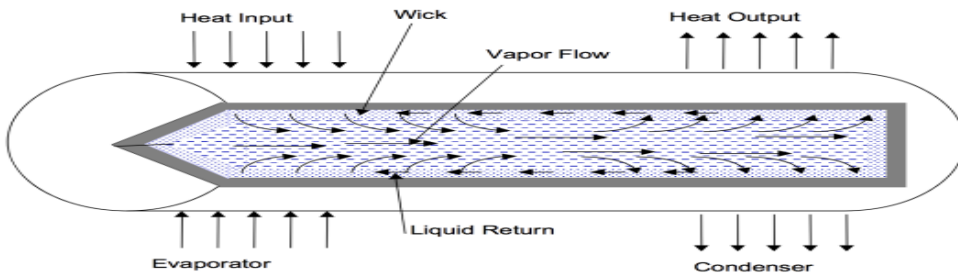
## Principles

- Heat pipes are heat transfer devices
- Utilize thermal conduction and phase transition of a working fluid
- Two-phase (boiling and condensation) allow large heat transfer with minimal  $\Delta T$  between heat source and sink

## Benefits

- Excellent heat transfer rates
- Completely passive, no power sources, no moving parts (other than fluid)
- Completely sealed system, no exchange of fluid or interfacing systems

### Capillary (wicking)



## Heat Transfer Rates

- Very high heat transfer rates are possible due to energy of phase transitions
  - Heat capacity of water:
    - $\sim 4.22 \text{ kJ/kgK}$  ( $100^\circ\text{C}$ )
  - Enthalpy of vaporization of water:
    - $\sim 2250 \text{ kJ/kg}$  ( $100^\circ\text{C}$ )

- Very high thermal conductivity
  - Thermal conductivity of solids
    - Aluminum ( $\sim 200 \text{ W/mK}$ )
    - Copper ( $\sim 400 \text{ W/mK}$ )
    - Diamond ( $\sim 1,000 \text{ W/mK}$ )
  - Effective thermal conductivity of heat pipes
    - $5,000 - 200,000 \text{ W/mK}$

- Very high heat transfer rates
  - Heat transfer rates of  $23,000 \text{ W/cm}^2$  have been achieved with lithium heat pipes
  - For comparison, the heat emitted from the sun is  $6,000 \text{ W/cm}^2$

Courtesy: Argonne National Lab

# Background

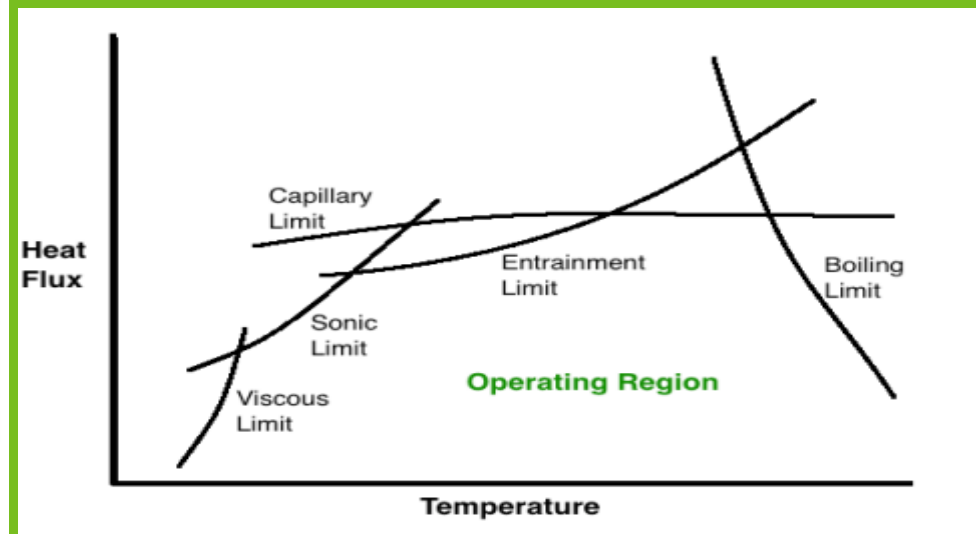
## ■ Limits

- **Viscous:** Near triple point or melting point of fluid, high viscosity prevents circulation back to the evaporator
- **Sonic:** At high power but low temperature, the vapor flow reaches sonic velocity, choking the flow
- **Entrainment:** High vapor velocity strips the liquid from the walls (larger concern for thermosyphons with no wick)
- **Capillary:** Capillary force is insufficient to overcome pressure drop
- **Boiling:** Rapid boiling and surface bubbles in the evaporator prevent condensate from entering and re-wetting



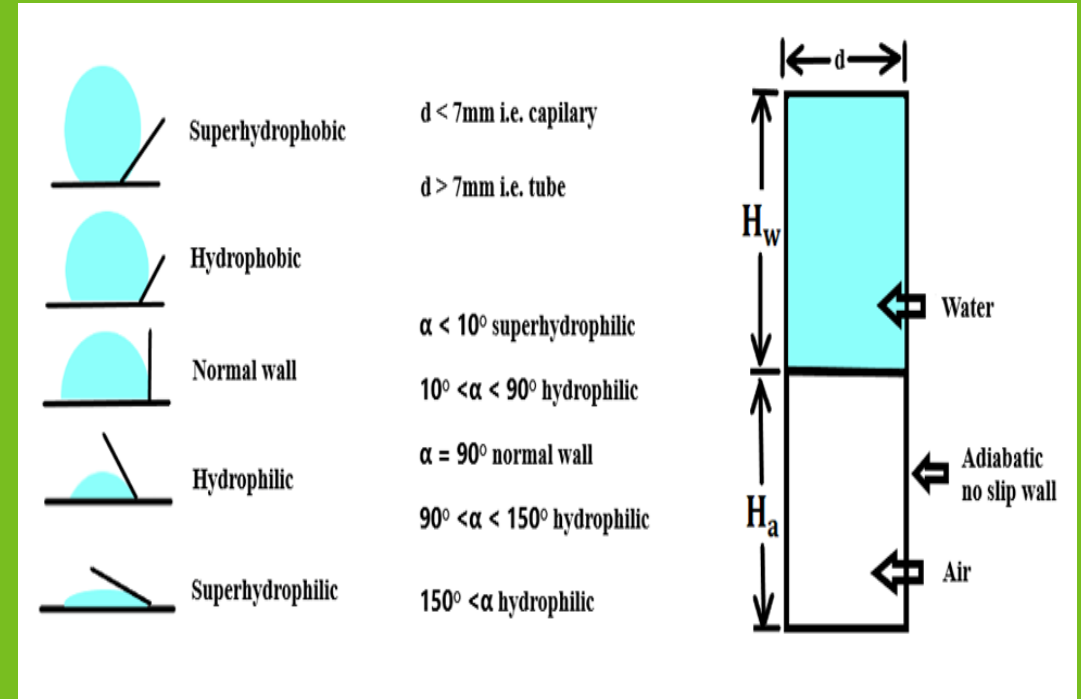
In this photo taken in the early 1960s, physicist George Grover tests a heat pipe.

| Fluid   | Approximate Operating Temperature Range (°C) | Heat of Vaporization (kJ/kg) | Heat Pipe Material |
|---------|--|------------------------------|--------------------|
| Helium  | -271 to -269                                 | ~20                          | SS, Titanium       |
| Ammonia | -75 to 125                                   | ~1,300                       | Aluminum, SS       |
| Water   | 1 to 300                                     | ~2,250                       | Copper, Titanium   |
| NaK     | 500 to 800                                   | ~2,500                       | SS                 |
| Sodium  | 500 to 1,200                                 | ~4,000                       | SS                 |
| Lithium | 1,000 to 1,825                               | ~21,000                      | Tungsten, Niobium  |



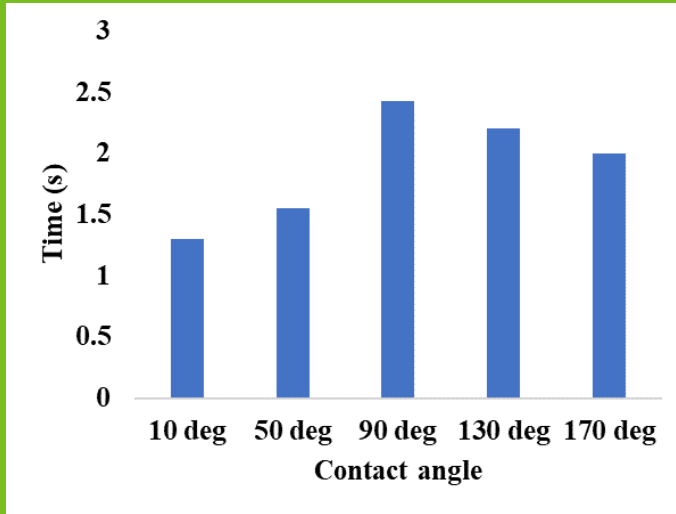
# Objective

- ❖ To check the effect of coatings on Rayleigh Taylor instability for heat pipes
- ❖ To check the drop-down performance of condensed liquids from monoliths to large diameter channels
- ❖ To check how gravitational heat pipes perform in different planets for space application
- ❖ To check different working fluids performance from light (water) to high viscous fluid (silicone oil)

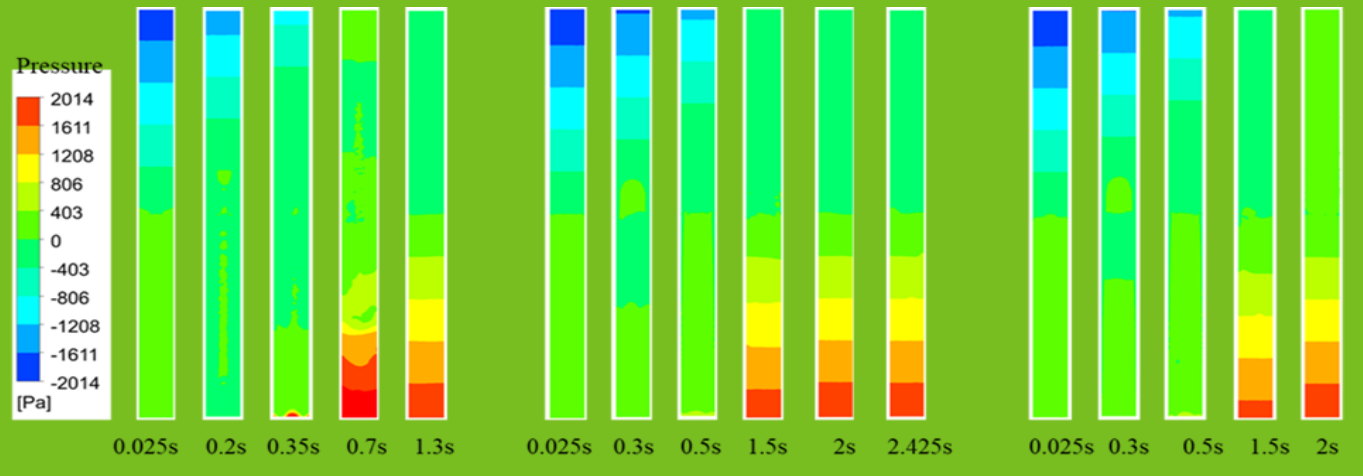
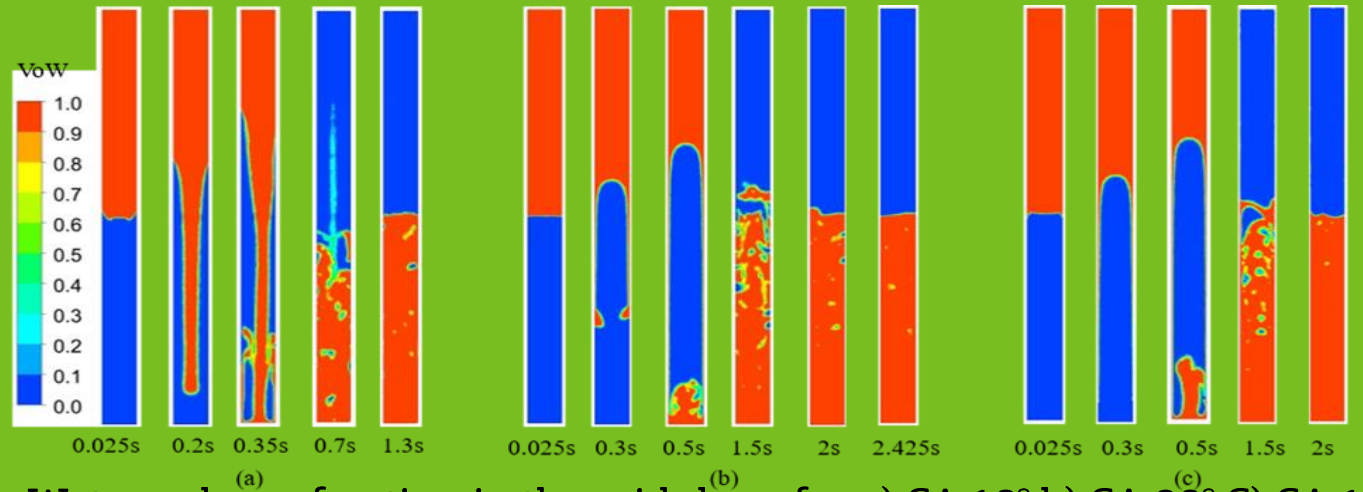


| Mesh size            | Dropping time |
|----------------------|---------------|
| 2.5 mm, 172102 cells | 2.61 s        |
| 1.5 mm, 481707 cells | 2.4 s         |
| 1 mm, 1028033 cells  | 2.42 s        |

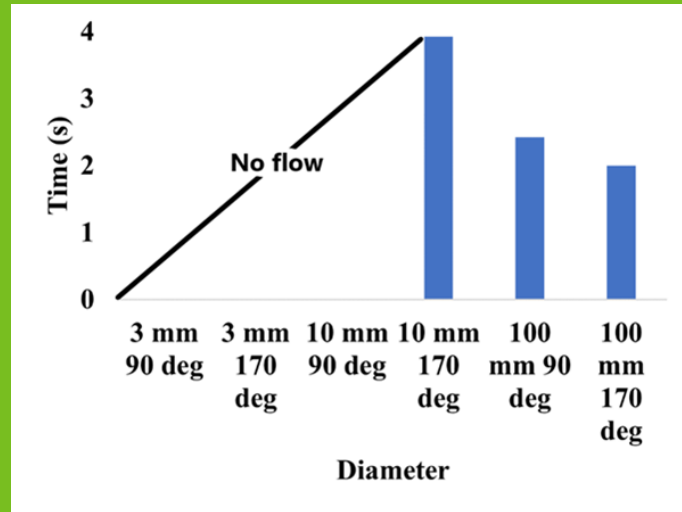
# Role of Contact Angle



- ❖ Drop down time is lower for super hydrophilic coatings
- ❖ Different flow nature for super hydrophilic coatings than normal and super hydrophobic walls
- ❖ Normal wall takes the longest time



# Role of Diameter



- ❖ No flow in capillaries
- ❖ Strong affinity between wall and water in super hydrophilic coatings
- ❖ Curved interface formation in capillary for super hydrophobic coatings. However, viscosity is still dominant.
- ❖ Flow happens when gravity force is dominant over viscosity and interface breaks up to initiate the flow

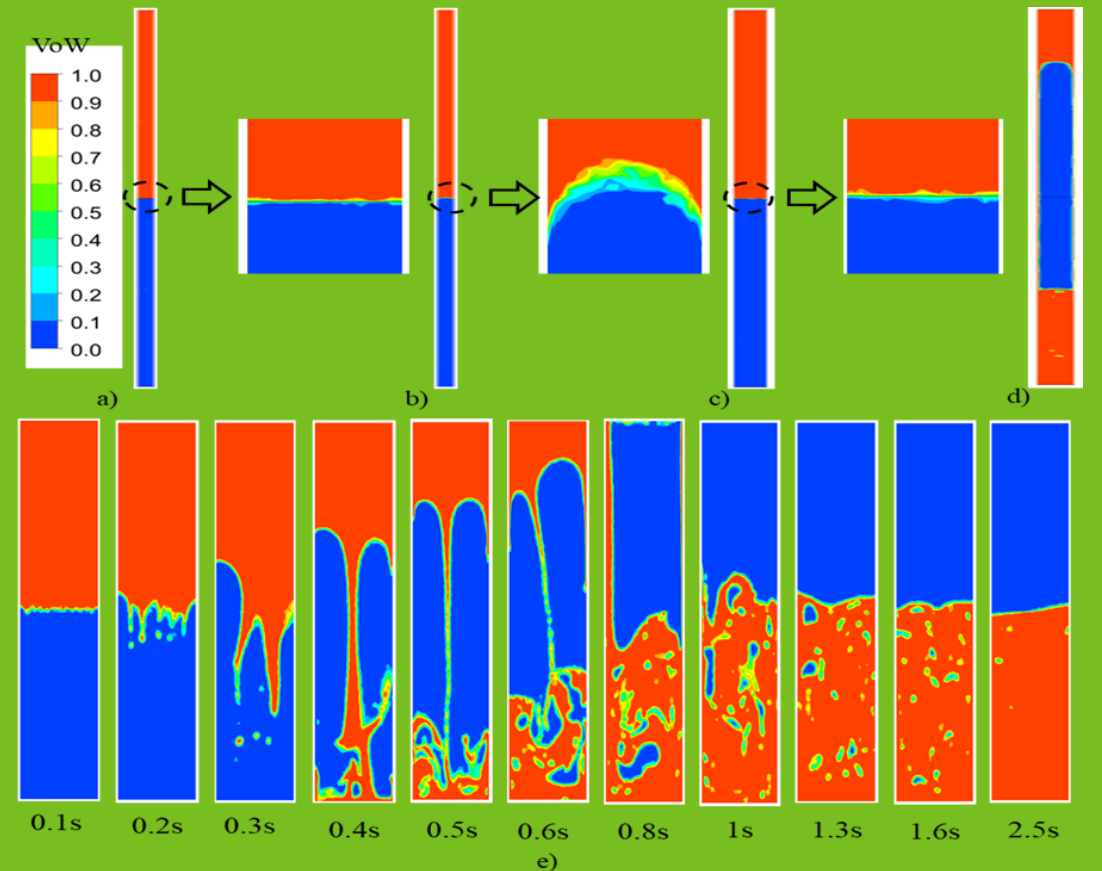


Figure: Water volume fraction for different diameter channels a)  $d=3\text{mm}$ ,  $\alpha=90^\circ$  b)  $d=3\text{mm}$ ,  $\alpha=170^\circ$  c)  $d=10\text{mm}$ ,  $\alpha=90^\circ$  d)  $d=10\text{mm}$ ,  $\alpha=170^\circ$  e)  $d=100\text{mm}$ ,  $\alpha=90^\circ$

# Role of Gravity

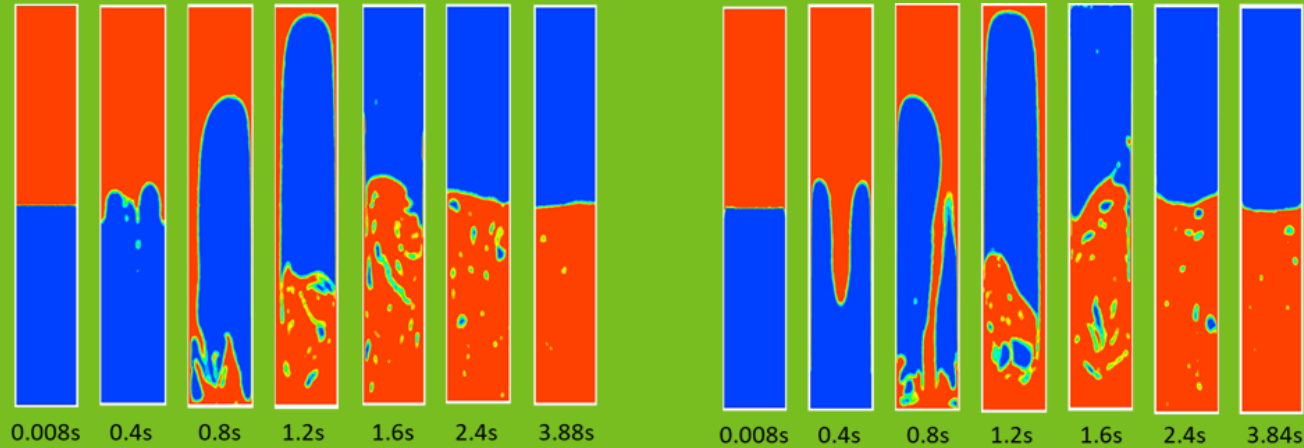


Figure: Water volume fraction for a)  $g = 9.81 \text{ m/s}^2$  b)  $3.84 \text{ m/s}^2$

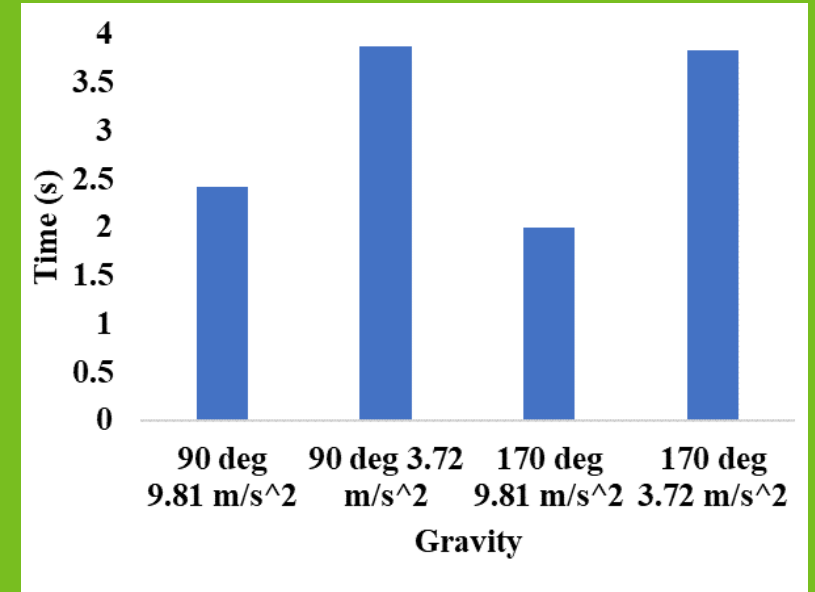


Figure: Gravity vs time

- ❖ Coating showed impact on drop down time
- ❖ Gravity doesn't show any impact on dropdown time

# Role of Viscosity

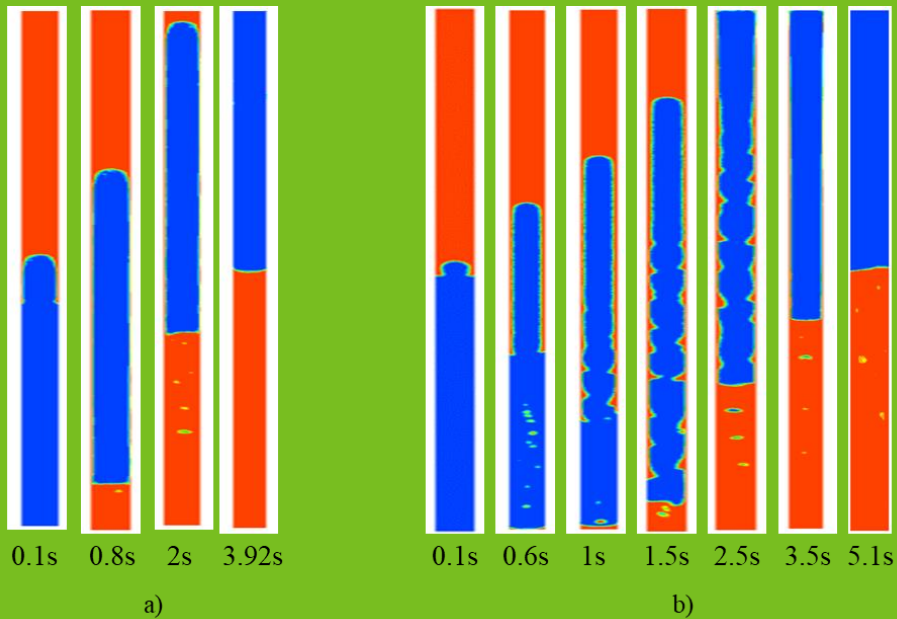


Figure: Water volume fraction for a) water flow b) silicone oil flow

- ❖ Water dropdown time is lower for than silicone oil
- ❖ Instability formation in silicone oil flow

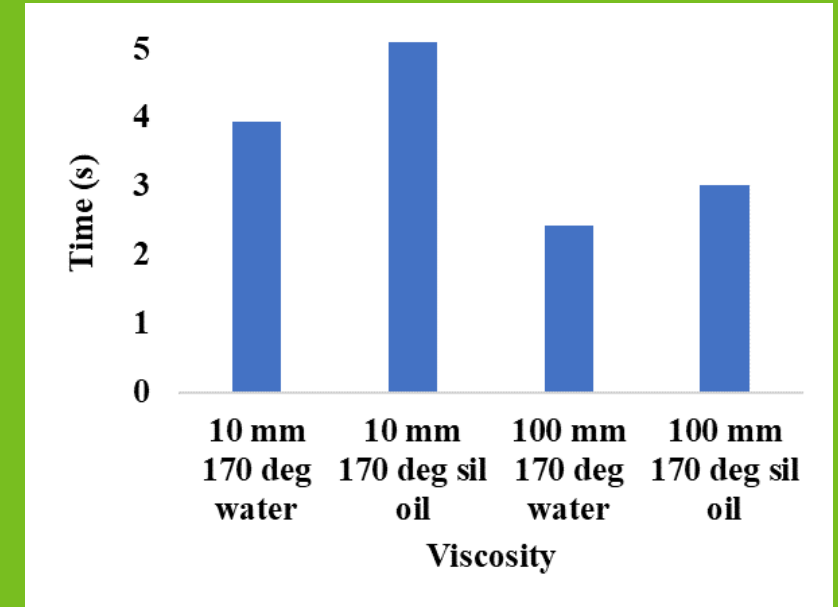


Figure: Viscosity vs time

- ❖ Instability might have negative effect in heat pipe performance such as choking



# Conclusions

- ❖ Five different wall coatings (super hydrophilic, hydrophilic, normal, hydrophobic and superhydrophobic) are computationally tested for capillaries to large diameter channels for assessment of Rayleigh Taylor instability
- ❖ Super hydrophilic coating showed the lowest dropdown time
- ❖ Normal and superhydrophobic walls showed similar flow nature
- ❖ Super hydrophilic materials showed good performance for large channels but blocks the flow in capillaries due to high affinity for water
- ❖ Hydrophobic and superhydrophobic materials showed consistent performance for different diameters
- ❖ High viscosity fluids has the chance to block the flow
- ❖ Flow in low gravity faces higher interface breakup but no change in dropdown time

Thank you

Any questions?